# **Monte Carlo simulation of terpolymerization**

**F. M. Mirabella Jr** 

*ARCO/Polymers Inc., Monroeville, Pennsylvania 15146, USA (Received 14 February 1977; revised 7 April 1977)* 

A simulation of terpolymerization, using the Monte Carlo method, and a computer program which performs the calculations for finite and infinite chain length conditions, are described. Terpolymer composition and sequence distributions are given as a function of chain length for two terpolymer systems. It was found that statistical equilibrium is achieved at chain lengths of about 100 units.

merization was described. The present paper describes a the monomers in the feed. There are nine propagation re-Monte Carlo simulation of terpolymerization. Little work actions which need to be considered in order to describe the has been done on the simulation of the stochastic growth of terpolymerization propagation steps, assumin has been done on the simulation of the stochastic growth of terpolymerization propagation steps, assuming that the ulti-<br>terpolymers. In this work the initiation and the propagation mate unit of a 'living' polymer chain so steps were included in a model which simulates the growth monomer unit is added next<sup>4</sup>. These nine propagation re-<br>of terpolymer chains of any arbitrarily specified length. A actions lead to six 'ultimate unit' reactivit computer program was used to calculate terpolymer compo- conditional probability expressions: sitions and monomer sequence distributions for finite chain length terpolymers, by the Monte Carlo method, and for infinite chain length terpolymers, by the usual probabilistic 1 method<sup>2,3</sup>.  $\overline{C_2}$   $\overline{C_3}$  (7)

### SIMULATION OF TERPOLYMERIZATION

Three distinct initiation reactions are needed to describe the initiation of the termonomers  $(M_1, M_2, and M_3)$  in a terpolymerization, assuming one initiation species  $(I^{\bullet})$ :

$$
\mathbf{I} \cdot + \mathbf{M}_1 \xrightarrow{k_{i1}} \mathbf{I} - \mathbf{M}_1 \tag{1}
$$

$$
I \cdot + M_2 \xrightarrow{k_{i2}} I - M_2 \cdot C_2 \qquad (2) \qquad C_3 \qquad r_{12} C_3
$$

$$
I^{*} + M_{3} \xrightarrow{k_{i3}} I - M_{3} \tag{3}
$$

where the initiation rate constants are  $k_{i1}$ ,  $k_{i2}$  and  $k_{i3}$ . The initiation rate constants are rarely known. The assumption made in this work was that the initiator selects between monomers 1, 2 and 3 only on the basis of feed composition and relative monomer reactivities toward the same radical. Thus, the initiation probabilities for processes  $(1)$  to  $(3)$ , respectively, are given by:

$$
P_{i1} = \frac{I_1 C_1}{I_1 C_1 + I_2 C_2 + I_3 C_3}
$$
(4) 
$$
P_{23} = \frac{1}{I_1 I_2 C_1 + I_2 C_2}
$$
(12)

$$
P_{i2} = \frac{I_2 C_2}{I_1 C_1 + I_2 C_2 + I_3 C_3}
$$
 (5)

$$
P_{i3} = \frac{I_3 C_3}{I_1 C_1 + I_2 C_1 + I_3 C_3}
$$
 (6) 
$$
P_{31} = \frac{I_3 C_2}{1 + \frac{r_{31} C_2}{r_{32} C_1} + \frac{r_{31} C_3}{C_1}}
$$

INTRODUCTION where  $I_1$ ,  $I_2$  and  $I_3$  refer to the normalized relative reactivities of monomers 1,2 and 3, respectively, toward the same radical In a previous paper<sup>1</sup> a Monte Carlo simulation of copoly- and, similarly,  $C_1$ ,  $C_2$  and  $C_3$  are the molar concentrations of mate unit of a 'living' polymer chain solely determines which actions lead to six 'ultimate unit' reactivity ratios<sup>4</sup> and nine

$$
P_{11} = \frac{1}{1 + \frac{C_2}{r_{12}C_1} + \frac{C_3}{r_{13}C_1}}
$$
(7)

$$
P_{12} = \frac{1}{1 + \frac{r_{12}C_1}{C_2} + \frac{r_{12}C_3}{r_{13}C_2}}
$$
(8)

$$
I^{+} + M_{1} \xrightarrow{k_{i1}} I - M_{1} \tag{9}
$$
\n
$$
P_{13} = \frac{1}{1 + \frac{r_{13}C_{1}}{C_{3}} + \frac{r_{13}C_{2}}{r_{12}C_{3}}}
$$
\n
$$
(9)
$$

$$
I^{+} + M_{3} \xrightarrow{k_{i3}} I - M_{3} \t\t(10)
$$
\n
$$
P_{21} = \frac{1}{1 + \frac{r_{21}C_{2}}{C_{1}} + \frac{r_{21}C_{3}}{r_{23}C_{1}}} \t\t(10)
$$
\n
$$
P_{11} = \frac{1}{1 + \frac{r_{21}C_{2}}{C_{1}} + \frac{r_{21}C_{3}}{r_{23}C_{1}}} \t\t(10)
$$

$$
P_{22} = \frac{1}{1 + \frac{C_1}{r_{21}C_2} + \frac{C_3}{r_{23}C_2}}
$$
(11)

$$
P_{23} = \frac{1}{1 + \frac{r_{23}C_1}{r_{21}C_3} + \frac{r_{23}C_2}{C_3}}
$$
(12)

$$
P_{31} = \frac{1}{1 + \frac{r_{31}C_2}{r_{32}C_1} + \frac{r_{31}C_3}{C_1}}
$$
(13)

POLYMER, 1977, Vol 18, September 925





\* See equations (4)-(6). <sup>†</sup> Values were calculated by normalizing the values given in ref 6 for each set of three monomers. ‡ Values obtained from ref 7

$$
P_{32} = \frac{1}{1 + \frac{r_{32}C_1}{r_{31}C_2} + \frac{r_{32}C_3}{C_2}}
$$
(14)

$$
P_{33} = \frac{1}{1 + \frac{C_1}{r_{31}C_3} + \frac{C_2}{r_{32}C_3}}
$$
(15)

where each probability,  $P_{jk}$ , refers to a chain ending in monomer *j* adding monomer *k*, and the reactivity ratios, monomer *j* adding monomer k, and the reactivity ratios, *Tables 2* and 3 present the results of the Monte Carlo simu-<br> $r_{ik}$ , are numbered as is customary<sup>5</sup>. The sum of each set of lations for the two terpolymer systems three equations (4) to (6), (7) to (9), (10) to (12), and (13) ly. These data show that as the chain length increases the to (15)is unity, effect of the initiation step vanishes and statistical equili-

culated before each event (using the current values of feed and greater, the agreement between composition and se-<br>composition and the various constants involved) and assigned quence distribution data obtained by simulatio composition and the various constants involved) and assigned quence distribution data obtained by simulation and in<br>a proportionate interval between 0 and 1, as described pre-<br>chain length data becomes good. This is simila a proportionate interval between 0 and 1, as described previously<sup>1</sup>. A random number generator is then used to pro- vious results in which agreement between copolymer simuduce uniformly distributed random numbers which deter-<br>mine the outcome of each initiation and propagation event<sup>1</sup>, lengths of about 300 units and greater<sup>1</sup>. mine the outcome of each initiation and propagation event<sup>1</sup>. A computer program was used to perform these calculations and to compute instantaneous and cumulative terpolymer compositions and monomer sequence distributions. The probabilities expressed in equations (7) to (15) were also used to compute the previously mentioned quantities for the infinite chain length terpolymers by the usual probabilistic method $^{2,3}$ . All computing was done on a CDC 175 computer. CONCLUSIONS A listing of the FORTRAN 4 extended program is available

The Monte Carlo simulation was performed for the ter-<br>polymer systems styrene/butadiene/methyl methacrylate<br>the model used in the simulation to predict the composition polymer systems styrene/butadiene/methyl methacrylate the model used in the simulation to predict the composition<br>(S/B/MMA) and styrene/vinyl acetate/methyl acrylate and monomer sequence distributions of chains of finite (S/B/MMA) and styrene/vinyl acetate/methyl acrylate and monomer sequence distributions of chains of finite<br>(S/VA/MA). The simulations were done for chains from 10 and depends on whether the model includes the maic (S/VA/MA). The simulations were done for chains from 10 length depends on whether the model includes the major<br>to 5000 units long and for infinite chain length. The simu-<br>governing factors of the polymerization. Further st to 5000 units long and for infinite chain length. The simu-<br>lations were done from zero conversion up to the desired<br>necessary in order to improve the Monte Carlo simulation lations were done from zero conversion up to the desired necessary in order to improve the Monte Carlo simulation<br>conversion in 0.5% molar conversion increments. Thus, in for ternolymerization by comparing data from simple conversion in 0.5% molar conversion increments. Thus, in  $\sigma$  terpolymerization by comparing data from simple simula-<br>the case of the S/B/MMA system, the growth of 170 chains tion models to experimental data and then modi was simulated from 0 to 85% molar conversion and in the models as indicated by the comparison. case of the S/VA/MA system the growth of 150 chains was simulated from 0 to 75% molar conversion, at each chain \* This choice was made because of available data. Relative reacti- length. *Table 1* gives the values of the constants used. The vities with highly electrophilic initiator radicals could be quite normalized relative reactivities of the monomers were cal-<br>different.

culated using values of the relative reactivities of the mono-<br> $\frac{1}{2}$ mers with the styrene radical<sup>6  $*$ </sup>.

### RESULTS AND DISCUSSION

*lations for the two terpolymer systems, mentioned previous-*In the Monte Carlo simulation these probabilities are cal- brium is approached. At chain lengths of about 100 units

on request.<br>The Monte Carlo simulation was performed for the ter-<br>wisualizing this extremely complex process. The ability tion models to experimental data and then modifying the

Table 2 Composition and sequence distribution data as a function of chain length for the styrene/butadiene/methyl methacrylate system *Table 2* Composition and sequence distribution data as a function of chain length for the styrene/butadiene/methyl methacrylate system



Monte Carlo simulation of terpolymerization: F. M. Mirabella Jr



Monte Carlo simulation of terpolymerization: F. M. Mirabella Jr

Table 3 Composition and sequence distribution data as a function of chain length for the styrene/vinyl acetate/methyl acrylate system

## *Monte Carlo simulation of terpolymerization: F. M. Mirabella Jr*

- *2 Ham, G. E. J. Polymer* 1977, 18, 705<br> *2 Ham, G. E. J. Polym. Sci, (A-2)* 1964, 2735<br> *3 Tosi, C. Eur. Polym. J.* 1970, 6, 161<br> *7*
- 
- 
- 4 Alfrey, T. Jr and Goldfinger, G. J. Chem. Phys. 1944, 12, 322
- REFERENCES 5 Ham, G. E. 'Copolymerization', (Ed. G. E. Ham), lnterscience, New York, 1964, p 32
- 1 Mirabella, F. M., Jr. *Polymer* 1977, 18, 705 6 Wailing, C. 'Free Radicals in Solution,' Wiley, New York, 1957,
	- 3 Total 18-119<br>
	3 Tolymer Handbook', (Eds J. Brandrup and E. H. Immergut),<br>
	2 Tolymer Handbook', (Eds J. Brandrup and E. H. Immergut),